Laser Flow Visualization," Proceedings of the New Orleans Conference on Laminar and Turbulent Boundary Layers, ASME, New York, Feb. 1984, pp. 41-51.

³Govindaraju, S. P. and Chambers, F. W., "Direct Measurements of Drag of Ribbon Type Manipulators in a Turbulent Bound-

ary Layer," AIAA Paper 86-0284, Jan. 1986.

⁴Lemay, J., Provencal, D., Gourdeau, R., Nguyen, V. D., and Dickinson, J., "More Detailed Measurements behind Turbulence Manipulators Including Tandem Devices Using Servo-Controlled Balances," AIAA Paper 85-0521, March 1985.

⁵Savill, A. M., "The Skin Friction Reduction Mechanisms of Flat Plate Turbulence Manipulators," Proceedings of the EUROMECH

1984 Colloquium, Saltsjobaden, Sweden, Aug. 1984.

⁶Westphal, R. V., "Skin Friction and Reynolds Stress Measurements for a Turbulent Boundary Layer Following Manipulation using Flat Plates," AIAA Paper 86-0283, Jan. 1986.

⁷Sahlin, A., Alfredsson, P. H., and Johansson, A. V., "Direct

Drag Measurements for a Flat Plate with Passive Boundary Layer Manipulators," Physics of Fluids, Vol. 29, Feb. 1986, pp. 696-700.

Motion of Bubbles in a Varying Pressure Field

Michael Mond*

Ben-Gurion University of the Negev, Beer-Sheva, Israel

I. Introduction

RECENTLY, there has been a growing interest in the properties of bubbly liquids. This interest ranges from the propagation of sound waves in liquids to the properties of bubbly liquid metals for various technological applications. 1-3,8 The dynamics of compressible bubbles in a liquid exhibit variations on two distinct time scales under various conditions. This behavior is caused by the natural volume oscillations of the bubbles, which are much faster than the motion of the liquid. As a result, the time step used in numerical calculations of bubbly flows is limited by the low period of the fast oscillations. This limitation can be removed by separating the flow variables into slow and fast components. By analytically finding the fast behavior and integrating over it, the time step can be significantly increased and is limited only by the much slower motion.

The separation of the flow variables into fast and slow components is carried out by the multiple-scale analysis. 4 The slow variations in the oscillation period and amplitude of the bubbles are determined by the requirement that no secular terms exist in any order of the equations of motion.

In Sec. II the behavior of a single bubble in a slowly varying pressure field is investigated. In Sec. III the equations of motion of bubbly flow are separated into slow variables and fast oscillations. The resulting equations are averaged over the fast time scale.

II. Single-Bubble Dynamics

The equation describing the dynamics of a single bubble in an unbounded liquid is given by5

$$R \frac{\mathrm{d}^2 R}{\mathrm{d}t^2} + \frac{3}{2} \left(\frac{\mathrm{d}R}{\mathrm{d}t}\right)^2 = \frac{P_g - P_\infty}{\rho_1} \tag{1}$$

where R is the radius of the bubbles, P_g its internal pressure, ρ_1 is the density of the liquid, and P_{∞} its pressure at infinity. It was assumed in Eq. (1) that the surface tension terms are small. Furthermore, in the case of a bubbly flow with a low gas content and small relative velocity between the bubbles and the liquid, Eq. (1) can still be used where P_{∞} is replaced by the liquid's pressure next to the bubble P. Whereas Eq. (1) describes the fast oscillations of the bubbles that are on time scale t_b , the pressure P varies on a much slower time scale denoted by t_1 . Thus Eq. (1) is given by

$$R \frac{\mathrm{d}^2 R}{\mathrm{d}t^2} + \frac{3}{2} \left(\frac{\mathrm{d}R}{\mathrm{d}t}\right)^2 = \frac{P_g - P(\tau)}{\rho_1} \tag{2}$$

where $\tau = \epsilon t$ and

$$\epsilon \approx t_b/t_1$$
 (3)

For a steady-state flow, ϵ can be estimated according to

$$\epsilon \approx \frac{u_b |\nabla P|}{P\omega_0} \tag{4}$$

where u_b and ω_0 are the velocity and natural frequency of the bubbles, respectively, and $P/|\nabla P|$ is an estimation of a characteristic length for a change in the liquid's pressure.

For the internal pressure P_g we use the equation of state of an ideal gas. Thus

$$P_{g}/\rho_{1} = a/R^{3} \tag{5}$$

where a is a constant that depends on the temperature and the mass of the bubble. As was demonstrated by Plesset and Hsieh, Eq. (5) holds for a wide range of frequencies.

Before turning to the multiple-scale analysis, we notice that since the bubble is expected to oscillate with a varying frequency, it is of benefit to define the following new variable:

$$\zeta = \int_0^t \omega_0(\epsilon \xi) d\xi = \frac{1}{\epsilon} \int_0^t \omega_0(\eta) d\eta$$
 (6)

where the natural frequency is given by

$$\omega_0^2(\tau) = 3a/R_0^5(\tau) \tag{7}$$

and $R_0(\tau)$ is obtained by setting the right-hand side of Eq. (2) to zero and using Eq. (5). The natural frequency at a constant pressure is obtained by linearizing Eq. (2) around a static state. After using the new independent variable defined by Eq. (6), Eq. (2) is transformed into the following equation:

$$R \frac{\mathrm{d}^2 R}{\mathrm{d}\zeta^2} + \epsilon \frac{\omega_0'}{\omega_0^2} R \frac{\mathrm{d}R}{\mathrm{d}\zeta} + \frac{3}{2} \left(\frac{\mathrm{d}R}{\mathrm{d}\zeta}\right)^2 = \frac{1}{\omega_0^2} \left(\frac{a}{R^3} - \frac{P}{\rho_1}\right) (8)$$

where the prime denotes differentiation with respect to the

We apply now the multiple-scale analysis. For this purpose we expand Eq. (8) in terms of the two time scales ζ and τ in the following way:

$$R(\zeta) = R_0(\tau) + \epsilon R_1(\zeta, \tau) + \epsilon^2 R_2(\zeta, \tau) + \dots$$
 (9)

$$\frac{\mathrm{d}R}{\mathrm{d}\zeta} = \frac{\partial R}{\partial \zeta} + \frac{\epsilon}{\omega_0} \frac{\partial R}{\partial \tau} \tag{10}$$

$$\frac{\mathrm{d}^2 R}{\mathrm{d}\zeta^2} = \frac{\partial^2 R}{\partial \zeta^2} + 2 \frac{\epsilon}{\omega_0} \frac{\partial^2 R}{\partial \zeta \partial \tau} + \frac{\epsilon^2}{\omega_0^2} \frac{\partial^2 R}{\partial \tau^2}$$
(11)

Received June 8, 1986; revision received Oct. 1, 1986. Copyright © American Institute of Aeronautics and Astronautics, Inc., 1986. All rights reserved.

^{*}Senior Lecturer, Pearlstone Center for Aeronautical Engineering Studies, Department of Mechanical Engineering.

Equations (9-11) are inserted into Eq. (8), and the resulting equation is solved order by order in ϵ . The zero order is automatically satisfied by the definition of $R_0(\tau)$. The first-order equation is given by

$$\frac{\partial^2 R_1}{\partial \zeta^2} + R_1 = 0 \tag{12}$$

The solution of Eq. (12) is given by

$$R_1(\zeta,\tau) = A(\tau) \cos \zeta + B(\tau) \sin \zeta \tag{13}$$

The coefficients A and B, which vary slowly in time, are determined by the requirement that the equation for R_2 does not include terms which might give rise to secular behavior. Thus the second-order equation is given by

$$\frac{\partial^{2} R_{2}}{\partial \zeta^{2}} + R_{2} = -\left[\frac{2R_{0}}{\omega_{0}} \frac{\partial^{2} R_{1}}{\partial \zeta \partial \tau} + \frac{\omega_{0}'}{\omega_{0}} R_{0} \frac{\partial R_{1}}{\partial \zeta} + \frac{3}{2} R_{0}' \frac{\partial R_{1}}{\partial \zeta}\right] + \text{NST}$$
(14)

The first three terms on the right-hand side of Eq. (14) contain all the terms that might give rise to a secular behavior of R_2 while the rest (nonsecular terms) contain $\cos 2\zeta$ and $\sin 2\zeta$. Thus the slowly varying coefficients are determined now by the requirement that the three first terms vanish:

$$2\frac{A'}{A} = -\frac{\omega_0'}{\omega_0} - 3\frac{R_0'}{R_0} \tag{15}$$

and the same equation for B. The solution of Eq. (15) is given by

$$A(\tau) = -A_0/(\omega_0^{1/2} R_0^{3/2}) \tag{16}$$

Using Eq. (6), we finally write

$$R_{1}(\zeta,\tau) = \frac{1}{\left[R_{0}(\tau)\right]^{\frac{1}{4}}} \left\{ A_{0} \cos\left[\frac{1}{\epsilon} \int_{0}^{\tau} \omega_{0}(x) dx\right] + B_{0} \sin\left[\frac{1}{\epsilon} \int_{0}^{\tau} \omega_{0}(x) dx\right] \right\}$$
(17)

where A_0 and B_0 are constants determined by the initial conditions.

An important result is immediately obvious, namely that if an oscillating bubble is moving into an area of increasing pressure, its equilibrium radius decreases, and hence the amplitude of the oscillations is enhanced. On the other hand, the oscillations of a bubble moving in the opposite direction of the pressure gradient are stable.

III. Averaged Bubbly Flow

The method described in the previous section can be used to eliminate the fast time scale from the equations that govern the motion of bubbles in a liquid. In order to show that, the following assumption are made: 1) the liquid is incompressible, 2) the bubbles move in the liquid with a constant velocity, 3) the number of bubbles per unit volume n_0 is a constant, 4) the relative velocity between the bubbles and the liquid is small, hence the bubbles are assumed to be spherical, and 5) the average distance between the bubbles is small, hence Eq. (1) can be used for describing the bubbles' radius. It is noted that not all the assumptions previously listed are necessary for the following discussion. Assump-

tions 1-3 are made in order to make the algebra more transparent and can be removed for a more general case. Under these assumptions, the equations that govern the motion of the bubbles in the liquid are

$$\frac{\partial}{\partial t}(1-\alpha) + \frac{\partial}{\partial x}[(1-\alpha)u] = 0 \tag{18}$$

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = -\frac{1}{\rho_1} \frac{\partial P}{\partial x}$$
 (19)

$$R \frac{d^2 R}{dt^2} + \frac{3}{2} \left(\frac{dR}{dt} \right)^2 = \frac{a}{R^3} - \frac{P}{\rho_1}$$
 (20)

where α is the void fraction and is given by $4\pi n_0 R^3/3$. A model similar to Eqs. (18-20) was introduced by Wijngaarden⁷ and discussed by Caflisch et al.⁸

As in Sec. II, a new independent variable ζ is defined by Eq. (6). In addition, a new space variable is defined by

$$\xi^* = \int_0^{x/u_b} \omega_0(\epsilon x) dx \tag{21}$$

It is more convenient, however, to transform to the frame of reference moving with the bubbles by

$$\xi = \xi^* - \zeta \qquad v = (u - u_h)/u_h \tag{22}$$

In terms of the new variables, Eqs. (18-20) become

$$\frac{\partial \alpha}{\partial \zeta} + v \frac{\partial \alpha}{\partial \xi} - (1 - \alpha) \frac{\partial v}{\partial \xi} = 0 \tag{23}$$

$$\frac{\partial v}{\partial \xi} + v \frac{\partial v}{\partial \xi} = -\frac{1}{\rho_1} \frac{\partial P}{\partial \xi}$$
 (24)

and Eq. (8). Similar to the temporal behavior of a single bubble, the spatial behavior is split into fast and slow variations. Thus a slow coordinate is defined by

$$\sigma = \epsilon \xi$$
 (25)

The following solutions are assumed for the dependent variables:

$$\psi = \psi_0(\sigma, \tau, \epsilon) + \sum_{n=1}^{\infty} \epsilon^n \psi(\sigma, \tau, \xi, \epsilon) \exp(in\zeta)$$
 (26)

The averaging process works as follows: Eq. (26) is inserted into Eqs. (23), (24), and (8). The resulting equations are then multiplied by $\exp(in\zeta)$ and integrated over a whole period in ζ . Each of the resulting equations is then solved order by order in ϵ . The lowest-order equations are

$$\frac{\partial \alpha_0}{\partial \tau} + v_0 \frac{\partial \alpha_0}{\partial \tau} - (1 - \alpha_0) \frac{\partial v_0}{\partial \sigma} = 0$$
 (27)

$$\frac{\partial v_0}{\partial \tau} + v_0 \frac{\partial v_0}{\partial \sigma} = -\frac{1}{\rho_1} \frac{\partial P_0}{\partial \sigma}$$
 (28)

where R_0 and α_0 are given by

$$R_0^3(\tau,\sigma,\epsilon) = a\rho_1/[P_0(\tau,\sigma,\epsilon)]$$
 (29)

$$\alpha_0 = (4\pi/3)n_0(R_0^3 + 3\epsilon^2 R_0 R_1^2) + \mathcal{O}(\epsilon^3)$$
 (30)

It is easy to show that the first-order solution that appears in Eq. (30) is given by

$$R_1 = R_1(\tau, \sigma, \epsilon) \exp(iv_0 \xi) \tag{31}$$

and R_1 is calculated in a similar way as outlined in Sec. II. From Eqs. (27-31), we notice two important results. First, the equations of motion that govern the bubbly flow are written in terms of τ and σ alone, which represent the slow temporal and spatial variations respectively. Thus, solving Eqs. (27) and (28) numerically, a larger time step can be used which is $1/\epsilon$ bigger than the time step needed for solving the original set of equations (18-20). Second, the fast oscillations affect the bulk motion of the two phases at least in order ϵ^2 .

IV. Conclusions

The existence of two distinct time scales in bubbly flows was used in order to integrate over the fast variations that occur due to the natural volume oscillations. First, the oscillations of a single bubble in a slowly varying pressure field were investigated. Using the multiple-scale technique it was shown that these oscillations are enhanced if the liquid's pressure is growing. Then, a procedure was introduced that averages the equations of bubbly flows over the fast oscillations.

As a result, a set of reduced differential equations is obtained which depend only on the slowly varying independent variables. This procedure enables the use of large time steps in numerical computations.

References

¹Mond, M., "Parametric Excitations of Instabilities in Bubbly

Flows," Physics of Fluids, Vol. 29, June 1986, pp. 1774–1778.

²Tan, M. J. and Bankoff, S. G., "Propagation of Pressure Waves in Bubbly Mixtures," Physics of Fluids, Vol. 27, June 1984, pp. 1362-1369.

³Crespo, A., "Sound and Shock Waves in Liquids Containing Gas Bubbles," *Physics of Fluids*, Vol. 12, Nov. 1969, pp. 2274-2282.

⁴Cole, J. D., Perturbation Methods in Applied Mathematics, Blaisdell, Waltham, MA, 1968, pp. 79-120.

⁵Lamb, H., *Hydrodynamics*, Dover, New York, 1945, p. 120.

⁶Plesset, M. and Hsieh, D., "Theory of Gas Bubbles Dynamics in Oscillating Pressure Fields," Division of Engineering and Applied Sciences, California Institute of Technology, Pasadena, CA, Rept. No. 85-16, March 1962.

Van Wijngaarden, L., "On the Equations of Motion for Mixtures of Liquid and Gas Bubbles," Journal of Fluid Mechanics, Vol.

33, May 1968, pp. 465-474.

⁸Caflisch, R., Miksis, M., Papanicolau, G., and Ting, L., "Effective Equations for Wave Propagation in Bubbly Liquids," Journal of Fluid Mechanics, Vol. 153, Jan. 1985, pp. 259-273.

Optimization of Equivalent Periodic Truss Structures

M. Lajczok*

Martin Marietta Denver Aerospace, Denver, Colorado

Introduction

IMPLE beam models of complex periodic space struc-S IMPLE beam models of complex periods tures can be effectively used to optimize the dimensions of the structural members. This could result in enormous cost

savings as well as provide the analyst with valuable insights into the behavior of complex periodic space structures. However, care must be exercised when computing member loads from these simple beam models. Specifically, for a long cantilever periodic space structure, the fundamental frequency and tip displacement can be accurately determined using a Bernoulli-Euler beam. However, the member loads can be accurately calculated only by using a Timoshenko beam.

Behavior of Truss Structure

The cantilever truss shown in Fig. 1 is taken to illustrate the difference obtained by using a Bernoulli-Euler beam and a Timoshenko beam. The member properties are as follows:

$$E = 71.7 \times 10^9 \text{ N/m}^2$$
 $L = 75 \text{ m}$ $\rho = 2768 \text{ kg/m}^3$ $A_c = 80 \times 10^{-6} \text{ m}^2$ $A_c = 7.5 \text{ m}$ $A_g = 60 \times 10^{-6} \text{ m}^2$ $A_g = 5.0 \text{ m}$ $A_d = 40 \times 10^{-6} \text{ m}^2$

where A_c , A_g , and A_d are the cross-sectional areas of the vertical, horizontal, and diagonal members, respectively. These dimensions and properties were chosen so that the truss could be considered a Bernoulli-Euler beam. One load condition, as shown in Fig. 1, is imposed: P = 200 N.

Using the approach developed by Sun et al., the equivalent beam properties can be obtained as follows:

$$AE = 2A_d E(\beta^3 + \gamma) \tag{1}$$

$$EI = 0.5EA_cL_g^2 \tag{2}$$

$$KAG = 2A_d E\alpha^2 (1 - \alpha^2)^{1/2}$$
 (3)

where

$$\alpha = L_g/L_d$$
, $\beta = L_c/L_d$, $\gamma = A_c/A_d$

The design problem to be solved here can be stated as follows: Find the dimension of the members such that the mass of the structure

$$m = \{2n[A_cL_c + A_dL_d] + (n+1)[A_gL_g]\}\rho$$
 (4)

where n, the number of periodic structures, is minimized subject to the following constraints:

1) Frequency Constraint

$$(\omega/\omega_0) - 1 \ge 0 \tag{5}$$

where ω is the fundamental frequency of a Bernoulli-Euler beam and is given by

$$\omega = [1.875/L]^2 \sqrt{EIL/m_r} \tag{6}$$

and $m_r = m - A_g L_g \rho$ (since base girder fixed mass is not participating). Also, ω_0 is the minimum allowable fundamental frequency, which for this problem is 5 rad/s.

2) Tip Displacement Constraint

$$1 - (\Delta_x / \Delta_{\text{max}}) \ge 0 \tag{7}$$

where Δ_x is the tip displacement given by

$$\Delta_x = PL^3/3EI$$
 (Bernoulli-Euler)

$$\Delta_x = (PL^3/3EI) + (PL/KAG)$$
 (Timoshenko) (8)

Also, Δ_{max} is the maximum allowable tip displacement, which for this problem is 0.4 m.

Received March 24, 1986, revision received June 27, 1986. Copyright © American Institute of Aeronautics and Astronautics, Inc., 1987. All rights reserved.

^{*}Staff Engineer, Structural Analysis.